Singapore International Water Week April 2022:

Hydrogen Circular Economy: Viability, Scalability, & Risk For Water Industry

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Introduction

Integration of sustainable hydrogen (H_2) production with capture of associated greenhouse gases & carbon, & local use of co-products:

- facilitate an emerging circular economy,
- help the water industry to achieve net zero carbon emissions,
- supply chain security for water treatment chemicals.

In particular, green hydrogen & co-products such as O_2 , O_3 and H_2O_2 are essential within an emerging circular economy:

- sustainable fuels,
- chemical synthesis feedstocks,
- oxidising agents for AOP.



Introduction

Wastewater treatment plants produce large quantities of recycled water & biogas, providing co-location opportunities for hydrogen production and alternative reuse prospects:

- Water source concerns for sustainable hydrogen,
- Reinforces circular economy principles of wastewater as a valuable resource,
- Avoids potentially harmful wastewater discharges to the environment,
- Reduces capital expenses by using existing infrastructure, land, & supply chains.
- + recycled-water-based drought schemes may have potential for hydrogen production during non-drought periods.



Challenge

While hydrogen production opportunities may add significant value to WWTP operations:

- Associated risks
- Viability?
- Scalability?
- Urban and regional perspectives?
- Value proposition of a hydrogen circular economy to water industry stakeholders?

Objective

- Understand these concerns and provide site-specific guidance to prospective utilities aiming to address technical considerations of feasibility, scalability and viability
- Formulate a decision tree to support utility decision-making and risk assessment.





Economic viability

Understand the economic viability of hydrogen production:

- Projected future demands for hydrogen & associated supply chain
 - The global hydrogen industry is expected to increase 40% by 2030, with Australia aiming to become a leading exporter of hydrogen, with potential export values of \$5.7bn by 2040.
 - To accelerate the development of a hydrogen economy and transition to a decarbonised future, we need to produce "clean" hydrogen at under AU\$2.00 per kilogram.





Economic viability

Understand the economic viability of hydrogen co-products:

- Projected future demands for co-products: O₃
 - The global O_3 market size was valued at USD \$ 880 million in 2016 and is expected to grow at a compound annual growth rate (CAGR) of 7.4% from 2017 to 2023.
 - \circ O₃ generators predominantly use air as the feed, but when oxygen is used, more ozone can be generated at lower energy consumption.
- Projected future demands for co-products: H₂O₂
 - Use in water industry; food, paper and pulp; chemical manufacturing; pharmaceutical & health; disinfectant products.
 - The global hydrogen peroxide market size was valued at USD 1.44 billion in 2020 and is expected to grow at a compound annual growth rate (CAGR) of 5.7% from 2020 to 2028.
 - Can production of co-products offset the production cost of H_2 , bringing the cost of H_2 production down to the targeted \$2/kg?



Technical viability

The technical viability of recycled-water-based hydrogen production also presents many research questions:

- Performance of electrolysers (which split water into hydrogen and oxygen in the presence of a catalyst)
 - low pH conditions ideal for hydrogen reduction
- Volumes of (recycled) water required
- Optimal operating conditions
- Impacts of contaminants in wastewater:
 - organic compounds
 - metal ions
 - nutrients
 - inorganic debris



Principles of electrochemical water splitting



Technical viability: WaterRA factsheet

https://www.waterra.com.au/ r11390/media/system/attrib/file/2690/WaterRA FS 1136 HydrogenEconomy.pdf



Background

Excess electrical energy generated by renewable sources including photovoltaic systems during devight hours could be used to power electrochemical water splitting to produce hydrogen (H,) and hydrogen perceite (H,O,), both of which are essential chemicals for the emerging hydrogen economy as foals, feedstacks in chemical sy ribeau, or additing agents in advanced acideton processes. Water spifting inalizonally uses freshe das which is already a scarse resource in ource in many countries including Australia. Additional consumption of frashwater countries including Australia. An effortation consumption of transmister for this parpears will increase operational costs of production and places additional streames on water resources. In major Australian when smars, larger outmans of macyclast australiant (WWTPA) and generated by controllated manipple automatic transmistrat plants (WWTPA), which and pravide available alternative water ascence for future electrolysis. A potential disadvantage emerges when considering the potent undesirable side effects of residual conteminants within DWW, which uncessmels are structs or massas communicate within HWW, which may reduce H, and H, Q, modelson efficienties and reduce electrolyse blespin. The modeled within quality for this process is thereby informed by the key importing that impute electrochemical H/H,Q, production using WWQ satisfications goldelines for electrochemical H/H,Q and WHTT

Principles of electrochemical water splitting



Figure 1. Schematic of the electrachemical water splitting process for HJH, D, garantion

Hydragen is set althurity e energy carrier due to its high energy density and lack of polluting by-products. Hydrogen produced vie water splitting Equation 1) can be stored transported, then acidsed as an energy acutes to achieve a carbon-mained cycle. Another etheckive product of water splitting is hydrogen persode (Equation 2 and 3) which can be utilized as a sustainable codetion reagent within advanced codetion processes or as an energy source for fuel cells. By connecting the electrocies with a renewable power source in series, H₂ is produced by hydrogen reduction at the cathode (HER, Equation 1) while H₂O₂ is an absorbed generative other from paygen reduction reactions (DBR, Equation 2) at the cathode

Updated 6 July 2021



respective excitations concritered RWDR Frequences XI at the seconds III to accide proton sectionings membrane alectrolysers (Figure 1), the generalized protons at the anode are transported through a proton exchange membrane (PEM) to satisfy the electrochemical half reactions at the reference (reset) to basing one was reconstructed as managed as the distribution. If why (F)(C), evaluation, a memory metasactical values (re-distribution of the second efforts fews attempted to address this through actempter studies of entrato nave anterropeo to estimas nave tracago economic ascess of Sax-cast electrocologists for efficient energy senter production (5,4). For PDM week electrolyca, enterence (in stability of electrocols and perform escharge membranes is also colocal to implementing the process for long-term and lange-scale usess.[5]

2H'+2# +H_(E_=0V vs.RHE)	(HER, Expansion 1)
$O_{j}+3H^{j}+3w \twoheadrightarrow H_{j}O_{j}\left(E_{ij}=+0.66Vv\approx RHE\right)$	(ORR, Equation 2)
$2H_{2}O+2H\rightarrow H_{2}O_{3}+2H^{\prime}\left(ED_{3}+L^{7/2}V\times aRHE\right)$	(WOR, Equation 3

Collebrate Innovate Impact



Impacts of electrolytes

Electrolytes pass impacts or reactor kinetics and electrode additively participating in electrochemical reduc processes and influencing mass rafer rates [6]. While conventional electrolysers work best within a haits or loss of the rest of the second of the second seco reprint the printings (print) is the original magnetization of the magnetization of the printing of the print tend to dignole at colourne pitt values, which places constrains on the long-term tellefailty of electrolysers. Here resulted pitt values toald avoid the potential destructurion source introduced by taunic electrolytes, so slong with afterts to develop consistent materials also the side of constraint and age and the side of the side of the

to addition to the influences of pitt aduble ions and molecules in electrolytes have been reported to have agrificant impacts on the efficiency of electrochemical mactions. The electrocatelyst layers of electrocyters have a person structure. HER, ORR and WOR reactions

Quality of recycled water

Table 1. Classes of recycled water and corresponding standards for biological treatment and pathagen reduction [10].

Water quality	UNR	Class A	Class B	ClassC
Turbidity	NIU	<2	6	
pH	-)	6.9*	6.91	6.91
Brachemical avygon domend (BOD)	mg0.	10	20	20
Suspendezi adilda (325)	uiĝ().	÷.	30	30
Residual chilonne	mg/t.	1	-	÷
E.col	200/700 mil	< 10 E cm2	100 E ank	1000 E a

Use of RWW from WWTP's presents as a potential solution to the hads volumes of wein negated for electrochemical $H_1(H,Q)$ evolution. In the Australian Goldelina for Water Recycling, singled water is defined as weiner that two been invatial to the two purpose standards for a people. explications (10). The Environment Protection Authority, Victoria provides Wmshold values of physical-chemical weter spalling (br example, turbility and BOD] and E. coli limits for biological inand partogen reduction (Halle 1) [H]. While the mapping of pollute wastenator are effectively nerved in the current wastenable trade processes, small errounts of contentinents (say, metal tons, organic components, tuttients, etc.) nimein in RWW (10). This wale range of patiential importance introduces a need to assess the focalifying of RWW as an electrolytic medium, which first requires the identification of kay importing in recyclicit water and the threahold concentrations at which ferences in electrolytic processes can be setticipated.

Electrolytic systems powered by renewable energy for the production of H, and H, O, may qualit the development of suchariable water treatment processes and the detection of all additions of access a second processes and the second proceses and the second processes and the second processe of key impurities in RWW and an assuument un their impacts on electricitanical processes are receivery to ensure the feedfally of electrocommutal processes an inclusion to advance the interval of a laborary negotiation for electrocommutation and a laborary Constanting then yours and constantiation of high constantiants in included water with Thurstell's qualitation of electrocommutation and a laborary an electrolysis of lengths and a positive weathy of the laborary for electro-works and a laborary of a laborary and a laborary of electronic states and electronic and with Thurstell's trappedies to facilitation servings of them in allocation for electro-works and a laborary of electronic states and electronic states and electronic and with the one to appende to facilitation servings of them in allocation of electronic states and electronic state selvanced exclution processes for water treat

can only occur at the spatially confined alter around the triariance

between the catelyst layers and the proton membranes, called triple phase boundaries (3PE), where knowers, reactants and electrically

contented califysits contact. The markets sizes of electrophermics contractor catalysts contact. The nucleon values of telephonetermails machines highly depend on the properties of TPMs and the proton transport ability of PDMs. Previous studies have abready shown that electrocontalysts and membranes in electrolysess are assorphible to

head-water importion, particularly cattors including Net, Ce¹⁴, Co¹⁴ and Fe¹⁵ 36, 03, While the mechanism of the metallic cattor passoring has

the "sign of which the measurements in the measurement cannot parametering the end yet frame high understands, if a generality basic will have these calores are obtained for a societary and a postare mendatures and the tectories in calculated layers, reducing the proton mediaty and increasing the over patiential of a calculated and modes. The active sites of electrocontely in the over the second second

can also be blocked by prevences and other impartues due depeats within

Interconnected catalyst layer pores, decreasing the internat: reactivity of the electrocatalysts. Further others will be required to clenitly which concentrations of head water imputties are takenable in long term

operation electrolyser operations.

Summary

Acknowledgment - WaterRA Project 1136 team You Liu/X teamy Zhang & Son Latery (Monash University) Isabel Talina Silverne (Water Co

Li Geo (South East Weter), Antone Brazil (Verw Vallay Weter), Nick Croster (Melboorne Weter), Liem Vaughen & Anash Zemyed (Weter)(A) References

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Technical viability

3-year ARC linkage project: Sustainable Hydrogen Production from Used Water

Objectives 1. To gain an in-depth understanding of how existing electrolysers perform in the presence of water impurities, and develop guidelines for designing water electrolysers with high tolerance of water

- 2. To identify the water quality gap between the treated water from existing WWTPs and the required feed water for water electrolysis, and provide recommendations for WWTPs operation and potential upgrading;
- 3. To evaluate the technical feasibility of utilising the co-products from waster electrolysis in wastewater treatment, and develop frameworks for the integration between wastewater treatment and water electrolysis.



Technical viability: Impacts of impurities & mitigation strategies





Gas Diffusion Layer (GDL)

Bipola

Plate

Technical viability: Impacts of impurities & mitigation strategies



Technical viability

- Volumes of water required: Theoretically 9kg of H₂O to produce 1 kg H₂. At scale: estimated to be up to 90 kg electrolyser cooling
- Energy consumed for hydrogen production

Manufacturer	Technology Name	Operating Pressure	Hydrogen Flowrate	Energy Consumption	Operating Range	Water Consumption	Power	Electrical Efficiency	
	HOGEN S10	13.8 bar _g	0.265 Nm³/hr - 0.57kg/d	1 74 kWh/kg H ₂	0-100%	9.9 L/kg H ₂	1.1 kW	-	
-	HOGEN S20		0.53 Nm ³ /hr - 1.14 kg/d				2.2 kW	-	
Manufashunan 1	HOGEN S40		1.05 Nm ³ /hr - 2.27 kg/d				4.3 kW	-	
Manufacturer 1	H2	15 bar _g / 30 bar _g optior	2 Nm ³ /hr	81 kWh/kg H ₂	0-100%	10.2 L/kg H ₂	8.1 kW	-	
	H4		4 Nm ³ /hr	78 kWh/kg H ₂			16.1 kW	-	
	H6		6 Nm ³ /hr	76 kWh/kg H ₂			23.7 kW	-	
	ME 100/350	15 - 30 bar _g	15-46.3 Nm ³ /hr	55 kWh/kg H ₂	32-100%	14.4 L/kg H ₂	225 kW	73%	
	ME 450/1400	15 - 30 bar _g	42-210 Nm ³ /hr	53 kWh/kg H ₂	20-100%	13.8 L/kg H ₂	1 MW	74%	
	HCS 2MW	15 - 30 bar _g	420 Nm ³ /hr	<53 kWh/kg H ₂	20-100%	16 L/kg H ₂	2 MW	>74%	
Manufacturor 2	HCS 4MW	15 - 30 bar _g	840 Nm ³ /hr			17 L/kg H ₂	4MW		
	HCS 10MW	15 - 30 bar _g	2100 Nm ³ /hr			$18 L/kg H_2$	10MW		
	S30/10	0 - 20 bar _g	0.22 Nm ³ /hr	-	-	29 kg/hr	1 kW		
	S30/30	0 - 20 bar _g	0.66 Nm ³ /hr	-	-	87 kg/hr	3 kW	78%	
	S30/50	0 - 20 bar _g	1.10 Nm ³ /hr	-	-	145 kg/hr	5 kW		
	HyLYZER 200		200 Nm ³ /hr		F 100%				
	HyLYZER 250		250 Nm ³ /hr	<55 KW0/Kg H ₂					
Manufacturer 3	HyLYZER 400	30 bar _g	400 Nm ³ /hr	<54 kWh/kg H ₂		5 - 100%	9 L/kg H ₂	-	-
	HyLYZER 500		500 Nm ³ /hr						
	HyLYZER 1000		1000 Nm ³ /hr	<51 kWh/kg H ₂	5 - 125%				
Manufacturar 4	SILYZER 200	35 bar	225 Nm ³ /h	-	-	17 L/kg H ₂	1.25 MW	60-65%	
ivianuracturer 4	SILYZER 300	-	1300 kg/hr	-	0-100%	10 L/kg H ₂	~70 MW	>75.5 %	

Scalability of production processes

- The scalability of production processes is also a key concern:
 - Regional utilities: many plants distributed across a large geographic area.
- The risks associated with utility involvement in a hydrogen circular economy are also poorly defined:
 - o Core business of a water utility?
- From a sustainability perspective a key potential risk is the allocation of water for hydrogen production in regions where water resource availability is subject to extreme variability due to climate change.
 - In this context, how can we not only secure water for electrolysis but continue to meet accessibility and affordability for other uses?





Scalability:

WaterRA water industry consortium



SCALING GREEN HYDROGENCRC

Water "core partnership" workshop May 6th 2022 (online) - Themes:

- Water sources and their social licence;
- Technology needs for water reuse and beneficial co-products;
- Co-location opportunities (including renewable energy generation) and Integrated planning.

Contact me to join the workshop: arash.zamyadi@waterra.com.au



Conclusion

- For successful integration of hydrogen and oxidant production into existing and newly developed water/wastewater treatment facilities, research questions regarding viability, scalability, sustainability and risks must be addressed.
- The potential gains are however promising, and adaptation of novel technologies for water reuse could facilitate a significant improvement in the sustainability and resilience of water treatment processes.



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WHO ARE

The co-location of hydrogen production at existing wastewater treatment plants may reduce capital expenses by using existing infrastructure, land, and supply chains.

Australian Water Association 63

Water Researc



Thank you

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